

# Silica-supported zirconocene/(perfluorophenyl)borate catalyst for propylene polymerization DRIFTS study of the catalyst formation and surface species

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## Abstract

IR spectroscopy has been used to study the interaction of silica with  $\text{PhNEt}_2$  (N) and  $\text{B}(\text{C}_6\text{F}_5)_3$  (B) and subsequent interaction of the support  $\text{SiO}_2/[\text{N} + \text{B}]$  with dimethylzirconocene  $\text{Me}_2\text{Si}(\text{2-Me-Ind})_2\text{ZrMe}_2$  ("Zr"). The data were obtained on the composition of the surface compounds appeared at both stages of catalyst synthesis.

It has been shown that (B) and (N) interact with OH groups of silica to form ionic pair  $[\text{H}-\text{NR}_3]^+[(\text{C}_6\text{F}_5)_3\text{B}-\text{O}-\text{Si}\equiv]^-$  (IP-1). Cation fragment of this pair contains highly reactive N–H bond with a.b. at  $3230\text{ cm}^{-1}$ . It has been found that N–H groups in a part of IP-1 complexes react with neighboring OH groups of silica by hydrogen bonding that gives complexes IP-2. It has been shown that "Zr" complexes interact both with complexes IP-1 and IP-2. As "Zr" reacts with IP-1, zirconium ionic complexes IP-3 containing Zr–Me bond are formed on silica. These complexes are suggested to be the precursor of the polymerization active sites. The reaction of "Zr" with IP-2, most likely, produces surface zirconium compound containing no Zr–Me bonds and inactive for propylene polymerization.

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**Keywords:** FTIRS; Supported zirconocene catalysts; Perfluoroarylborate activator; Propylene polymerization

## 1. Introduction

Metallocenes when used in combination with suitable activating agents (polymethylalumoxane (MAO) or perfluoroarylborate activators (FAB)) are extremely active catalysts for alkene polymerization [1,2]. The studies of homogeneous metallocene systems proved that dimethyl zirconocene derivatives react with MAO or FAB to produce ionic pairs of composition  $[\text{Cp}_2\text{ZrMe}]^+[\text{B}(\text{C}_6\text{F}_5)_4]^-$  or  $[\text{Cp}_2\text{ZrMe}]^+[\text{Me-MAO}]^-$  [3–6], which are assumed to be the precursors of the active sites at polymerization.

Supported metallocene catalysts are considered the most promising for practical applications. Common approach to synthesize these catalysts consists in supporting metallocene complexes on silica modified with MAO [7–9].

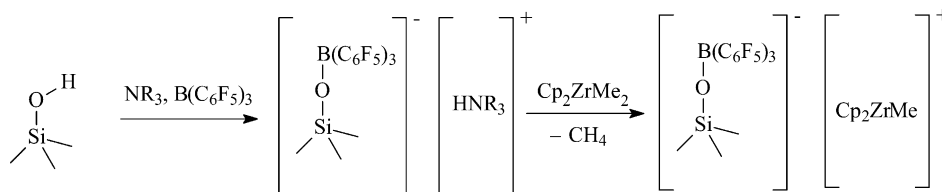
One of the methods to synthesize of MAO-free supported metallocene catalysts has been patented by Exxon Chem. Co. [10]. According to this patent and Refs. [11–15,24,25], supported ionic pairs are formed at the treatment of silica with alkyl aniline and *tris*-pentafluorophenyl boron followed by supporting of dimethylzirconocene (Scheme 1).

The composition and structure of surface species  $[\text{HNR}_3]^+[(\text{C}_6\text{F}_5)_3\text{BOSi}\equiv]^-$  has been investigated by IR and multinuclear solid-state NMR spectroscopies [24]. It has been shown that the unique  $[\text{HNR}_3]^+[(\text{C}_6\text{F}_5)_3\text{BOSi}\equiv]^-$  fragments are formed at highly dehydroxylated silica, whereas two sorts of surface sites: free silanol groups and ionic species  $[\text{HNR}_3]^+[(\text{C}_6\text{F}_5)_3\text{BOSi}\equiv]^-$  are formed at lower dehydroxylated silica.

IRS and solid-state CP-MAS  $^{13}\text{C}$  NMR studies [25] confirm that zirconocene ( $\text{Cp}^*\text{ZrMe}_3$ ) reacts primarily with the surface anilinium cation as it shown in Scheme 1.

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Scheme 1. Proposed scheme of MAO-free supported catalyst [10,11].

In the present work, we have used FTIRS in diffuse reflection (DRIFT) modes in more detail to study the reaction of silica with  $\text{PhNET}_2$  and  $\text{B}(\text{C}_6\text{F}_5)_3$  and subsequent reaction of the support obtained with dimethylzirconocene  $\text{Me}_2\text{Si}(\text{2-Me-Ind})_2\text{ZrMe}_2$ . DRIFTS is very effective method for study of real catalyst samples in powder form. In this case, the same catalyst samples are used both for polymerization and study of the surface species by DRIFTS. So it is more reliable way to consider the correlation between data on the surface species and activity at polymerization and analyze the effect of preparation details on the surface species and activity. We have studied the composition of the surface compounds formed at both stages of catalyst formation by means of DRIFTS mainly. The data on the catalyst performance in propylene polymerization are presented as well.

## 2. Experimental

The experiments were performed using the “break seal” technique.

$\text{Me}_2\text{Si}(\text{2-Me-Ind})_2\text{ZrMe}_2$ ,  $\text{PhNET}_2$ ,  $\text{B}(\text{C}_6\text{F}_5)_3$  and  $\text{SiO}_2$  (MS Davison 952, specific surface area  $310 \text{ m}^2/\text{g}$ , pore volume  $1.8 \text{ cm}^3/\text{g}$ ) were donated by Exxon-Mobil.

### 2.1. Synthesis of support

The measured sample of silica was heated in air at  $500^\circ\text{C}$  for 3 h, then placed into a quartz ampoule and dehydroxylated in vacuum at  $800^\circ\text{C}$  for 3 h. In some case, silica was dehydroxylated in vacuum at  $400$  or  $600^\circ\text{C}$  for 3 h.

$\text{SiO}_2/\text{B}(\text{C}_6\text{F}_5)_3$  and  $\text{SiO}_2/\text{PhNET}_2$  samples have been prepared by treating of silica with toluene solutions of  $\text{B}(\text{C}_6\text{F}_5)_3$  (molar ratio of  $\text{B}:\text{OH} = 1.2$ ) and  $\text{PhNET}_2$  (molar ratio of  $\text{N}:\text{OH} = 1.2$ ), respectively. The suspension was agitated for 1 h at room temperature and then washed out with toluene and dried in vacuum.

$\text{SiO}_2/[\text{PhNET}_2/\text{B}(\text{C}_6\text{F}_5)_3]$  sample has been synthesized as following. Silica was treated with toluene solution of  $\text{PhNET}_2$  (molar ratio of  $\text{N}:\text{OH} = 1.2$ ) at room temperature. The suspension was agitated for 1 h, then  $\text{B}(\text{C}_6\text{F}_5)_3$  was added to adjust  $\text{B}:\text{OH} = 1.2$ . The suspension was agitated for 1 h, then washed out with toluene four times and dried in vacuum at room temperature.

### 2.2. Synthesis of catalyst

Support  $\text{SiO}_2/[\text{NET}_2\text{Ph}/\text{B}(\text{C}_6\text{F}_5)_3]$  was treated with toluene solution of zirconocene  $\text{Me}_2\text{Si}(\text{2-Me-Ind})_2\text{ZrMe}_2$  adjusting molar ratios of  $\text{Zr}:\text{OH} = 1.25, 0.7$  and  $0.4$  at room temperature. The suspension was agitated for 0.5 h, the catalyst was washed out with toluene four times and dried in vacuum at room temperature.

### 2.3. Studies of chemical composition of supports and catalysts

#### 2.3.1. DRIFT study

The samples of supports and catalysts in a form of dry powders were placed into a special cell for DRIFT measurements under vacuum. The DRIFT spectra are presented in a form of Kubelka-Munk function [16]:

$$F(R) = \frac{(1 - R)^2}{2R} \quad (1)$$

where  $R$  is the reflection coefficient.

The DRIFT spectra were recorded on a Shimadzu FTIR-8300 spectrometer with DRS-8000 diffusion attachment in the  $400\text{--}6000 \text{ cm}^{-1}$  range with a resolution of  $4 \text{ cm}^{-1}$ .

#### 2.3.2. IRS study (transmission mode)

The silica powder was pressed into tablets (mass typically  $\rho = 10\text{--}15 \text{ mg}/\text{cm}^2$ ). The silica tablet was heated in air at  $500^\circ\text{C}$  for 1 h, then placed in a special cell and dehydroxylated at  $800^\circ\text{C}$  for 1 h at a pressure below  $2 \times 10^{-2}$  Torr. Dehydroxylated sample was cooled to room temperature and treated as described below. The samples of  $\text{SiO}_2/\text{B}(\text{C}_6\text{F}_5)_3$  and  $\text{SiO}_2/\text{PhNET}_2$  were produced by treating of silica tablets with toluene solutions of  $\text{B}(\text{C}_6\text{F}_5)_3$  (molar ratio of  $\text{B}:\text{OH} = 40$ ) and  $\text{PhNET}_2$  (molar ratio of  $\text{N}:\text{OH} = 40$ ), respectively.

The sample of  $\text{SiO}_2/[\text{PhNET}_2/\text{B}(\text{C}_6\text{F}_5)_3]$  was prepared as follows. The silica tablet was treated with toluene solution of  $\text{NET}_2\text{Ph}$  ( $\text{N}:\text{OH} = 40$ ) for 30 min, then the toluene solution of  $\text{B}(\text{C}_6\text{F}_5)_3$  ( $\text{B}:\text{OH} = 40$ ) was added. After 30 min the solution was decanted and the tablet washed out with toluene three times and dried under vacuum. Then the IRS measurements were performed.

The sample  $\text{SiO}_2/\text{BCl}_3$  has been prepared by treatment of silica with  $\text{BCl}_3$  ( $0.4 \text{ atm BCl}_3$ ) into the cell. The tablet was kept in  $\text{BCl}_3$  at  $400^\circ\text{C}$  for 0.5 h, then the cell was vacuumed

to  $2 \times 10^{-2}$  Torr at 400 °C. Then the treatment of the sample by  $\text{BCl}_3$  was repeated.

The IR spectra were recorded on a Shimadzu FTIR-8300 spectrometer in the 400–6000  $\text{cm}^{-1}$  range with a resolution of 4  $\text{cm}^{-1}$ .

#### 2.4. Studies of chemical composition

The content of aluminium and boron in the samples have been determined by means of inductively coupled plasma-atomic emission spectrometry (ICP-AES) as described in [17].

#### 2.5. Polymerization

The catalysts were tested in propene slurry polymerization in a steel autoclave (1.0 L) under the following conditions: catalyst loading 0.03–1 g, heptane (250 mL), temperature 70 °C, propene pressure 4 bar, co-catalyst  $\text{Al}(\text{i-Bu})_3$  (0.72 mmol/L), 2 vol.% of  $\text{H}_2$ , polymerization for 30 min.

### 3. Results and discussion

#### 3.1. The study of silica interaction with $\text{B}(\text{C}_6\text{F}_5)_3$ and $\text{NET}_2\text{Ph}$

First we have studied the interaction of silica dehydroxylated at 800 °C with individual FAB components ( $\text{B}(\text{C}_6\text{F}_5)_3$  and  $\text{PhNET}_2$ ). Fig. 1 presents the DRIFT spectra of  $\text{SiO}_2/\text{B}(\text{C}_6\text{F}_5)_3$  and  $\text{SiO}_2/\text{PhNET}_2$  samples.

Small decrease of intensity of a.b. at 3745  $\text{cm}^{-1}$  (terminal Si–OH groups) and appearance of the broad a.b. at 3720 and 3640  $\text{cm}^{-1}$  are observed after treatment of silica with  $\text{B}(\text{C}_6\text{F}_5)_3$  (Fig. 1, spectra 1 and 2). These new bands are attributed to hydrogen-bonded OH groups resulting from the reaction of terminal Si–OH groups with fluoroaryl groups in  $\text{B}(\text{C}_6\text{F}_5)_3$ . Besides, the DRIFT spectrum of  $\text{SiO}_2/\text{B}(\text{C}_6\text{F}_5)_3$  sample contains a set of a.b. at 3100–2700  $\text{cm}^{-1}$  range, originating from stretching vibrations of C–H of toluene used as a solvent. According to the data of chemical analysis (Table 1), boron content in  $\text{SiO}_2/\text{B}(\text{C}_6\text{F}_5)_3$  is very low (0.07 wt.%) that agreed with insignificant decrease of intensity of the a.b. at 3745  $\text{cm}^{-1}$ . The chemical analysis and DRIFTS data allow suggestion that  $\text{B}(\text{C}_6\text{F}_5)_3$  is fixed on the support surface owing to hydrogen bonding of Si–OH and fluoroaryl groups.

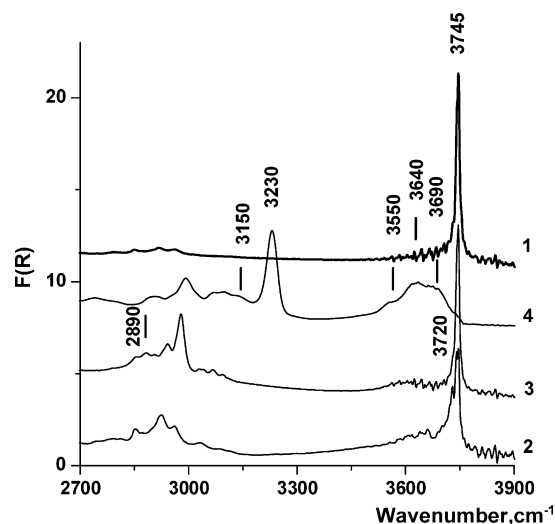


Fig. 1. DRIFT spectra of (1)  $\text{SiO}_2(800)$ , (2)  $\text{SiO}_2(800)/\text{B}(\text{C}_6\text{F}_5)_3$ , (3)  $\text{SiO}_2(800)/\text{Et}_2\text{NPh}$  and (4)  $\text{SiO}_2(800)/\text{Et}_2\text{NPh}/\text{B}(\text{C}_6\text{F}_5)_3$ .

The intensity of a.b. at 3745  $\text{cm}^{-1}$  also slightly decreases after treatment of silica with  $\text{PhNET}_2$  (Fig. 1, spectra 1 and 3). Broad and little intensive a.b. with a maximum at 3640  $\text{cm}^{-1}$  (hydrogen-bonded Si–OH groups) are appeared. Besides, the spectrum displays a set of a.b. at 2700–3100  $\text{cm}^{-1}$  range, characteristic for C–H stretching vibrations in Et and Ph groups and toluene molecules. These results suggest that  $\text{PhNET}_2$  adsorbed on silica fails to react efficiently with terminal OH groups. Only insignificant part of OH groups forms surface compounds due to hydrogen bonding. However, even low-efficient reaction of  $\text{NET}_2\text{Ph}$  with OH groups seems to weaken the SiO–H bond and thus facilitate subsequent reaction of silanol group with borate.

After successive treatment of silica with  $\text{PhNET}_2$  and  $\text{B}(\text{C}_6\text{F}_5)_3$  the a.b. at 3745  $\text{cm}^{-1}$  disappears while new a.b. at 2800–3100, 3150, 3230, 3550, 3640 and 3690  $\text{cm}^{-1}$  appear (Fig. 1, spectrum 4). a.b. at 2800–3100  $\text{cm}^{-1}$  can be attributed to the stretching vibrations of C–H bonds in organic molecules. a.b. at 3500–3730  $\text{cm}^{-1}$  are characteristic for stretching vibrations of hydrogen-bonded Si–OH groups originated from the reaction of terminal OH groups with the adsorbed molecules.

The presence of a.b. at 3150 and 3230  $\text{cm}^{-1}$  in the spectrum of  $\text{SiO}_2/[\text{PhNET}_2/\text{B}(\text{C}_6\text{F}_5)_3]$  is of key importance in the context of the present study. According to Refs. [20–22,24], these bands can be attributed to N–H stretching vibrations

Table 1

Data on boron content in the samples  $\text{SiO}_2/\text{X}$

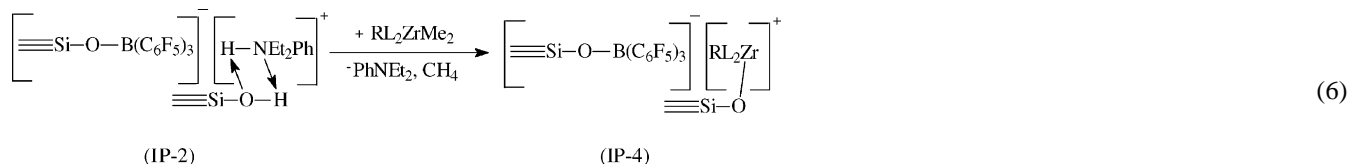
No.	X	B ( $\mu\text{mol/g}$ ) (wt.%)	[OH]/[B]	Zr $\mu\text{mol/g}$ (wt.%)	[OH] <sup>a</sup> /[Zr]	[Zr]/[B]
1	$\text{BCl}_3$	364 (0.4)	1.04	–	–	–
2	$\text{B}(\text{C}_6\text{F}_5)_3$	63.6 (0.07)	5.98	–	–	–
3	$\text{PhNET}_2 + \text{B}(\text{C}_6\text{F}_5)_3$	210 (0.23)	1.8	–	–	–
4	$\text{PhNET}_2 + \text{B}(\text{C}_6\text{F}_5)_3 + \text{Zr}$	210 (0.23)	1.8	198 (1.8)	1.92	0.94

<sup>a</sup> OH groups content in initial silica calculated according to IRS data is 380  $\mu\text{mol/g}$  [18].









We cannot exclude the reaction between hydrogen-bonded Si–OH groups and zirconocene complex with formation of inactive  $\mu$ -oxo-zirconium compounds. But this reaction is probably insignificant because the intensity of a.b. at 3630 and 3700  $\text{cm}^{-1}$  slightly decreases. Most part of SiOH groups is inaccessible for zirconocene due to steric hindrance of the bulky supported boron activator.

Table 1 shows the data on the chemical composition for the support  $\text{SiO}_2/[\text{N} + \text{B}]$  and catalyst  $\text{SiO}_2/[\text{N} + \text{B}]/\text{“Zr”}$ . It is seen that boron content in the support and catalyst is the same. That means that FAB in (IP-1) and (IP-2) surface species is tightly bound to silica surface. Molar ratio of Zr/B in catalyst  $\text{SiO}_2/[\text{N} + \text{B}]/\text{“Zr”}$  is close to unit ( $\text{Zr}/\text{B} = 0.94$ ). Thus, the data of chemical analysis are consistent with the DRIFT results and reactions (5) and (6).

The above results were obtained at the studies of catalysts prepared by supporting of excessive amount of zirconocene ( $\text{Zr}/\text{B} = 1.96$ ). We have studied the  $\text{SiO}_2/[\text{N} + \text{B}]/\text{“Zr”}$  samples synthesized at different Zr/B ratios.

Fig. 5 presents the DRIFT spectra of the catalysts prepared by supporting of different amount of “Zr” on  $\text{SiO}_2/[\text{N} + \text{B}]$  support. It is seen that after treatment of support with “Zr” at ratio  $\text{Zr}_{\text{in}}/\text{B} = 0.53$ , the intensities of a.b. at 3150 and 3550  $\text{cm}^{-1}$  decrease considerably, while intensity of a.b. 3230  $\text{cm}^{-1}$  ( $\nu_{\text{N-H}}$ ) remains almost the same (Fig. 5, spectra 1 and 2). As the ratio  $\text{Zr}_{\text{in}}/\text{B}$  increases, the intensities of a.b. at 3230  $\text{cm}^{-1}$  decreases (Fig. 5, spectra 3 and 4).

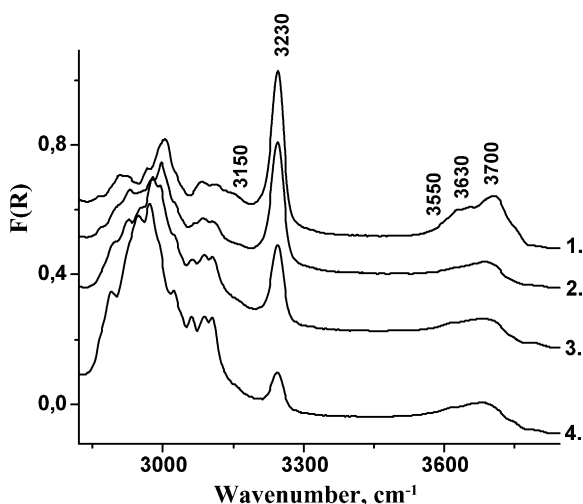


Fig. 5. DRIFT spectra of (1) support  $\text{SiO}_2/\text{PhNEt}_2/\text{B}(\text{C}_6\text{F}_5)_3$ , (2–4) catalysts  $\text{SiO}_2/\text{PhNEt}_2/\text{B}(\text{C}_6\text{F}_5)_3/\text{Me}_2\text{Si}(\text{2-Me-Ind})_2\text{ZrMe}_2$ : (2) 0.47% wt. Zr,  $\text{Zr}_{\text{in}}/\text{B} = 0.53$ , (3) 1.16 wt.% Zr,  $\text{Zr}_{\text{in}}/\text{B} = 1.26$ , (4) 1.8 wt.% Zr,  $\text{Zr}_{\text{in}}/\text{B} = 1.96$  ( $\text{Zr}_{\text{in}}$  – initial amount of zirconocene used for catalyst preparation).

Thus the DRIFT data allow suggest that as “Zr” is supported on  $\text{SiO}_2/[\text{N} + \text{B}]$  support, it reacts first with the surface complexes (IP-2) by reaction (6); if in excess Zr reacts with surface complexes (IP-1) via reaction (5).

The data on the chemical composition of the catalysts with different of zirconium content are listed in Table 3. It is seen that zirconium content in the catalysts was almost twice lower than zirconium loading. Even in sample 3 which was prepared by supporting twice lower amount of zirconocene with respect to boron content in the support ( $\text{Zr}_{\text{in}}/\text{B} = 0.53$ ) only a half of loaded zirconocene was detected in the catalyst. Most likely a part of zirconocene was involved into side reactions accompanying catalyst synthesis in particular into reaction with an amine released during reactions (5) and (6). This side reaction seems to produce soluble zirconocene–amine complex removed by catalyst washings.

Only the use of excess of zirconocene (Table 3, exp. 1,  $\text{Zr}_{\text{in}}/\text{B} = 1.96$ ) allows reaction of practically all (IP-1) complexes with zirconocene ( $\text{Zr}/\text{B} = 0.94$  in respective catalyst).

### 3.3. Catalytic properties of $\text{SiO}_2/[\text{N} + \text{B}]/\text{“Zr”}$ catalysts in propylene polymerization

Data on the activity of  $\text{SiO}_2/[\text{N} + \text{B}]/\text{“Zr”}$  catalysts differing by zirconocene in propylene polymerization are presented in Table 3. Obviously activity correlates with zirconium content in the catalyst. The catalyst with the highest zirconium content ( $\text{Zr}_{\text{C}}/\text{B} = 0.94$ ) showed the maximal activity. Thus, as zirconocene reacts with  $\text{SiO}_2/[\text{N} + \text{B}]$  first reaction (6) proceeds to form surface species which are inactive for propylene polymerization, and then surface species active for propylene polymerization are formed by reaction (5).

The data on the activity of catalysts differed by zirconium content are consistent with respective DRIFT data discussed above (Fig. 5).

Fig. 6 illustrates the kinetics of propylene polymerization with catalyst No. 1 from Table 3. The polymerization reaction was unsteady state (decay type). The maximal activity is observed for the first 5 min on-stream; then the catalyst deactivated rapidly. Meanwhile the nature of catalyst deactivation remains unclear.

Hydrogen input into reaction mixture increases greatly the initial activity but kinetic profile is decay type too (Fig. 6, curve 2). The effect of activation of propylene polymerization with zirconocene catalysts in hydrogen presence was observed in a number of researches [22,23].

Table 3  
Data on the composition and activity of catalysts SiO<sub>2</sub>/[N + B]/Zr in propylene polymerization

No.	Initial content of Zr		Catalyst composition			Yield <sup>b</sup> (gPP/g <sub>cat</sub> )	Activity <sup>c</sup> (kgPP/gZr min)
	Zr <sub>in</sub> (μmol/g)	Zr <sub>in</sub> /B <sup>a</sup> (mol/mol)	Zr (μmol/g)	Zr/B (mol/mol)	Zr/Zr <sub>1</sub> (mol/mol)		
1	470	1.96	198	0.94	0.42	400	57.4
2	263	1.26	127	0.61	0.48	268	23
3	110	0.53	52	0.25	0.48	10	2.2

Boron support content is 0.23 wt.%.

<sup>a</sup> Content of boron in the support is 0.23 wt.%.

<sup>b</sup> Yield of PP for 30 min.

<sup>c</sup> Initial activity for the first 5 min.

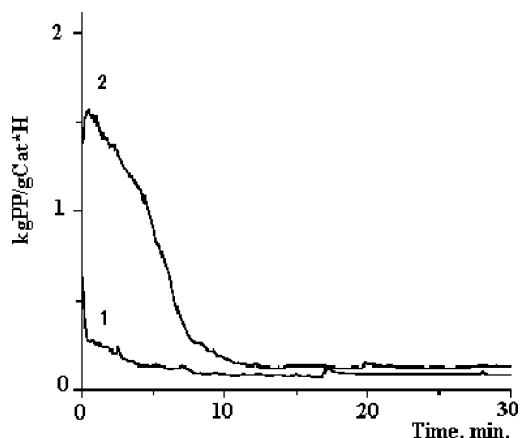


Fig. 6. The kinetic profile of catalyst SiO<sub>2</sub>/[N + B]/Zr in propylene polymerization at 70 °C, propylene pressure 4 bar, with Al(i-C<sub>4</sub>H<sub>9</sub>)<sub>3</sub> as scavenger: (1) polymerization without H<sub>2</sub> and (2) polymerization with H<sub>2</sub> (2 vol.% of H<sub>2</sub>).

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